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TECHNICAL REPORT

Synthesis of Large Area, Monocrystalline TiC as a Substrate for Heteroepitaxial Growth of $\beta\textsc{-SiC}$

Prepared by

Diamond Materials, Inc. 2820 East College Avenue State College, PA 16801

May 7, 1990

Principal Investigator
Richard Koba

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TECHNICAL REPORT

Synthesis of Large Area, Monocrystalline TiC as a Substrate for Heteroepitaxial Growth of \$\beta\$-SiC

1. INTRODUCTION

The purpose of this program is to demonstrate a novel process for synthesis of large area TiC single crystals. This SBIR program directly supports DoD efforts to develop monocrystalline β-SiC as a semiconductor material. β-SiC semiconductor devices offer the promise of one day replacing vacuum tubes as the source of microwaves for radar and communications. Because the cubic ("beta") polymorph of SiC is unstable at the sublimation temperature of SiC, the only methods demonstrated to produce large. single crystals of \(\beta \)-SiC have been heteroepitaxial growth by chemical vapor deposition (CVD). Monocrystalline Si, α -SiC, and TiC are all viable substrates for the heteroepitaxial growth of monocrystalline β -SiC. Of the three substrates, only TiC has been demonstrated to produce β-SiC films free of stacking faults, misfit dislocations, inversion domain boundaries, and double positioning boundaries. Additionally, TiC offers the advantage of being a good electrical conductor, exhibiting excellent ohmic contact to n-type \(\beta\)-SiC with low contact resistance. Therefore, \(\beta\)-SiC single crystal films grown on TiC substrates would be ideally suited for the fabrication of vertical FETs. Vertical FETs, such as the permeable base transistor (PBT), have achieved extremely high-power/high-frequency operation when fabricated in Si and GaAs.

CVD of monocrystalline β -SiC films on TiC has been limited by the unavailability of large area, TiC single crystals. TiC has numerous materials properties which make it difficult to grow as a large, monocrystalline boule by traditional crystal growing methods such as the float zone process. The economic viability of β -SiC semiconductors depends on the production of large-area TiC single crystals. Conventional TiC crystal growing methods (such as the float zone process) seem unlikely to synthesize large diameter, (i.e., up to 10 cm), monocrystalline boules of pure TiC free of pores, pinholes, and subgrain boundaries.

In this SBIR program, Diamond Materials, Inc. (DMI) is being funded to pursue a novel approach to the synthesis of large-area TiC single crystals. A summary of DMI's proposed procedure is as follows:

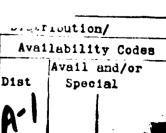


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- 1. Heteroepitaxial β -SiC will be grown by CVD on silicon wafers. The β -SiC will be grown to a thickness in excess of $\approx 30 \ \mu m$.
- 2. The silicon substrate will be selectively removed from the β -SiC film.
- 3. DMI will attempt to getter crystallographic defects from the outer $\approx 1 \mu m$ portion of the β -SiC single crystal by means of chlorinated oxidation. DMI will determine whether or not chlorinated oxidation can reduce the areal density of crystallographic defects on the β -SiC single crystal.
- 4. The gettered β -SiC single crystal surface will then be used as a substrate for the heteroepitaxial growth of TiC by chemical vapor deposition. The excellent lattice match of β -SiC to TiC should enable CVD of monocrystalline TiC.

2. ACCOMPLISHMENTS TO DATE

Diamond Materials, Inc. has focused its efforts on achieving the heteroepitaxial growth of monocrystalline β -SiC on silicon wafers. In summary, DMI has: (a) debugged its recently upgraded β -SiC CVD reactor, (b) learned how to etch silicon with HCl/H₂ mixtures to prepare the surface for β -SiC heteroepitaxy, (c) started experiments on CVD of β -SiC onto silicon using the source gas methyltrichlorosilane (MTS). DMI's next step is to grow a thick, monocrystalline β -SiC film on silicon and complete tasks 2, 3 and 4 as described in Section 1 above.

2.1 De-bug the β-SiC Reactor

As was described in the Progress Report (Sept. 7, 1989), DMI's \(\beta\)-SiC CVD reactor underwent extensive engineering modifications and additions, including: (a) a quick response gas handling system, (b) a completely redesigned "bell jar" assembly utilizing standard sized fused silica tubes, (c) a redesigned succeptor assembly, (d) an increase in the number of mass flow controllers (MFCs) to text, and (e) a heating system which maintains the MTS bubbler, the MTS MFC and the MAS stainless steel tubing at a constant temperature of 50°C to mitigate condensation of MTS downstream from the bubbler. (The boiling point of MTS is 66°C).

A major accomplishment to date has been mastery of the new gas flow logic. Several days were spent determining the necessary sequence of pneumatic valve positions and MFC actuation in order to ensure the proper flow. The MTS valving was especially complex since the special MTS bubbler (purchased from ATM, Inc.) is versatile, enabling direct flow of MTS impelled by MTS vapor pressure, or assisted flow of MTS using a H₂ carrier gas. After experimentation, it was decided to flow pure MTS through the MFC without any assistance from a carrier gas in order to maximize MTS flow accuracy and precision.

Minor problems were encountered and solved, such as replacement of defective MFC cables, cracked silica bell jars, and depletion of MTS supply. Since the β -SiC needed for this Phase I program does not have to be of semiconductor grade purity, DMI is employing reagent-grade MTS which is 98% pure packed in Ar. Although our β -SiC films are undoubtedly doped with residual nitrogen, the reagent-grade MTS is available in the necessary quantities without the weeks of lead time needed for a vendor to perform MTS purification.

2.2 Approach to 6-SiC Heteroepitaxy on Si

Based on conversations with experts, and by reading the literature, DMI felt that the optimal process for CVD of heteroepitaxial β -SiC on Si should be isothermal, or as close to isothermal as possible. The original procedure described by J. A. Powell and coworkers called for a two-step procedure where an initial thermal excursion is performed to etch the silicon in HCl/H₂, and a subsequent excursion is performed to first carburize and then deposit β -SiC from hydrocarbon + silane mixtures. The reason for the cool to room temperature after the HCl etch was probably to ensure complete purging of residual HCl from the CVD reactor before starting the β -SiC nucleation and growth step.

MTS, (CH3SiCl3), is a source gas which decomposes as:

$$CH_3SiCl_{3(v)} = SiC_{(s)} + 3HCl_{(v)}$$

Hence, deposition of β -SiC from MTS includes a concurrent HCl etching phenomenon which helps prevent the co-deposition of elemental silicon, graphite and α -SiC. DMI decided to deposit β -SiC immediately following the HCl etch step without cooling the substrate to room temperature.

The use of MTS should also make it unnecessary to carburize the silicon surface in order to nucleate a monocrystalline β -SiC layer. The carburization step was shown to generate defects in heteroepitaxial β -SiC in research performed by Molnar and Shirey of Naval Reseach Lab, (poster F8.7 presented at the Fall 1989 Materials Reseach Society meeting, "SEM Observation of Growth and Defect Formation on Heteroepitaxially Grown SiC on (100) Silicon.") Molnar and Shirey noted that a localized excess of reactive carbon at the silicon surface (i.e., during carburization) prompts outdiffusion of silicon from the near-surface region, creating "potholes" beneath the β -SiC film which exacerbate β -SiC film stress. Flowing a hydrocarbon over a silicon surface $\geq 1300^{\circ}$ C without also flowing a silicon source (e.g., silane) invites excessive outdiffusion of silicon from the substrate.

As demonstrated by Nishino and Saraie, ("Epitaxial Growth of 3C-SiC on a Si Substrate Using Methyltrichlorosilane," in <u>Amorphous and Crystalline SiC</u>, ed. by Harris and Yang, Springer-Verlag (1989) p. 45), carburization with a hydrocarbon is unnecessary to nucleate β-SiC when using MTS. Nishino and Saraie directly nucleated and grew heteroepitaxial β-SiC using 1 sccm of MTS plus 1 SLM of H₂ at 1300°C, (i.e., 0.1% MTS/H₂). Prior to MTS flow, they performed a separate temperature excursion for HCl/H₂ etching, which DMI believes is unnecessary.

DMI's goal is to develop a CVD procedure for β -SiC growth on Si composed of: (1) pump down to ultimate vacuum, (2) backfill with hydrogen to 250 torr and maintain that pressure for all subsequent steps. (3) heat up in H₂ to a fixed temperature (4) add HCl/H₂ to etch the silicon surface, (5) immediately switch off the HCl and add MTS/H₂ to nucleate and grow β -SiC, (6) turn off the MTS/H₂ and cool to room temperature in argon.

2.3 Hydrogen Etching Experiments

At the beginning of this program, DMI believed that the purpose of the HCl/H₂ etch step was simply to remove native oxide from the silicon crystal. Hence, an initial goal was to determine a heat up and etch sequence which would produce a flat, pinhole free silicon surface which would be free of native oxide immediately before commencing MTS flow.

Heat up experiments were performed in H₂. It was concluded that heat up in H₂ is preferrable to heat up in Ar because of the significantly higher thermal conductivity of H₂. Switching from Ar to H₂ would make it difficult to maintain substrate temperature continuity. Since the substrate is inductively heated, a sudden switch from

Ar to H₂ would cause the substrate temperature to plummet faster that the rf power supply could respond.

All experiments performed in the β -SiC reactor to date share a number of similarities. The total pressure is fixed at 250 torr and is maintained by a special high pressure throttle valve working in concert with a capacitance manometer. The wafers were cleaned according to the standard RCA procedure before being inserted into the reactor. It was observed that pure H₂ had the ability to etch the silicon surface. A series of runs were performed to determine the temperature to which silicon would be heated without sufferingH₂ etching. This temperature was determined to be 1000°C.

2.4 HCl/H2 Etching Experiments

After H₂ etching was investigated, DMI began performing HCl/H₂ etching experiments. Again, DMI believed that the reason why all published recipes for β -SiC heteroepitaxy included a preliminary etch was to remove native oxide. HCl/H₂ etching experiments were performed at temperatures between 1000 and 1300°C and at concentrations between 1 and 5% HCl diluted in H₂. It was observed that pitting of the silicon surface was almost always observed when flowing HCl except when the temperature was below 900°C.

After close microscopic examination of the etch pits, and re-examination of the published HCl etch recipes, it became clear that DMI had misinterpreted the true reason for the HCl etch step. All of DMI's H2 and HCl etch experiments were simply decorating crystalline defects present in the surface of silicon wafers. The chem-mechanical methods used to polish all semiconductor-grade silicon leaves the near-surface region of the silicon crystal riddled with stacking faults and other point and line defects. Defect gettering from the silicon surface is typically accomplished by HCl/O2 oxidation. DMI's mild HCl etch experiments were simply identifying the presence of crystalline defects near the wafer surface. DMI realized that the real motivation for the HCl etch prior to β -SiC growth is to etch away several microns of silicon to expose fresh defect-free silicon. Because the contribution of the hydrogen etch to the total HCl/H2 etch was minor, the pure H2 etch portion of the procedure was eliminated.

DMI obtained a desirable result by increasing the aggressiveness of the HCl etch procedure. In run 44, 5 secm of HCl plus 95 secm of H2 were run for 5 minutes at 1300°C, with cool down in argon. The result was the formation of a layer of silicon which had almost completely detached from the silicon surface. The silicon layer was several microns thick, and was bowed upward, still attached to the substrate at the center. In

run 46, the process conditions of run 44 (5% HCl/H₂ at 1300°C) were repeated for a longer time, 10 minutes, and resulted in complete removal of the defective layer of silicon. Figure 1 is a SEM micrograph of the flat bottom hole cut into the silicon wafer during run 46. The hole is \approx 5 μ m deep and has a rather smooth texture at its bottom. It is apparaent that the HCl had to remove the outer 5 μ m of silicon to reach a silicon region which etches at a uniform rate. Uniform etching over the area of the surface indicates a lack of point defects left behind in the silicon by the chem-mechanical polishing step.

The etch procedure developed in run 46 was then instituted for all subsequent MTS runs. An etch temperature of 1300° C was desirable since CVD of of heteroepitaxial β -SiC should occur at a similar temperature.

2.5 <u>β-SiC Growth Experiments</u>

A listing of the MTS growth experiments performed so far appears in Table 1. Each MTS growth experiment immediately followed the 5% HCl/H₂ etch procedure defined by run 46.

Table 1: \(\beta\)-SiC Growth Experiments.

	Flow (Duration	Temp.		
Run	Hydrogen	MTS .	% MTS	(min.)	(°C)
49	200	1	0.50	5	1300
52	300	1	0.33	5	1300
53	250	1	0.40	5	1300
59	300	3	1.0	5	1300
60	250	4.75	1.9	5	1300
63	250	4.75	1.9	5	1300-1400

SEM micrographs of the samples described in Table 1 appear as Figures 2 - 8. Comparing the figures, it is apparent that the thickness of the films is proportional to the MTS percentage. The figures also indicate the evolution of β -SiC film microstructure. Figure 7B shows the edge view of affilm. The β -SiC films grow in two stages. The initial stage is island growth of oriented β -SiC crystals. When seen in plan

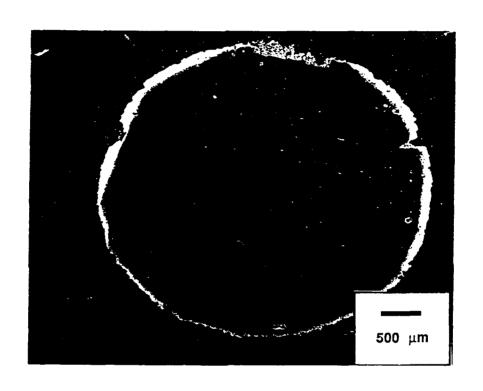


FIGURE 1. Run 46. SEM micrograph of flat-bottom crater in silicon created by 10 minutes of 5% HCl/H2 etching at 1300°C.

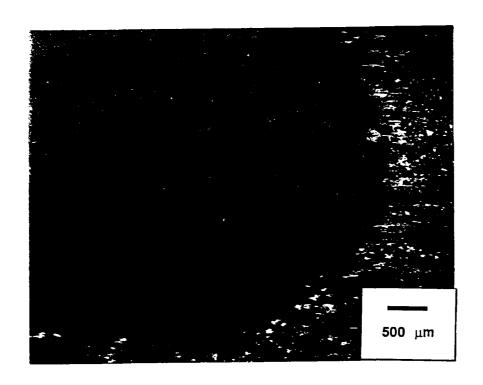
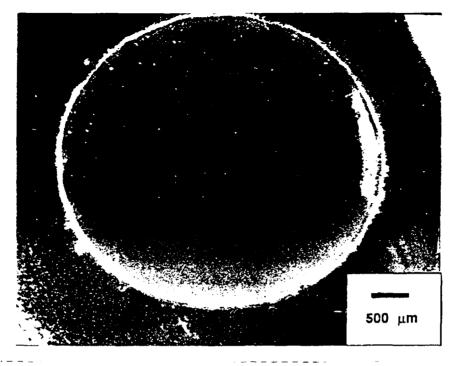


FIGURE 2. Run 49. SEM micrograph of film grown from 0.50% MTS/H2 at 1300°C.



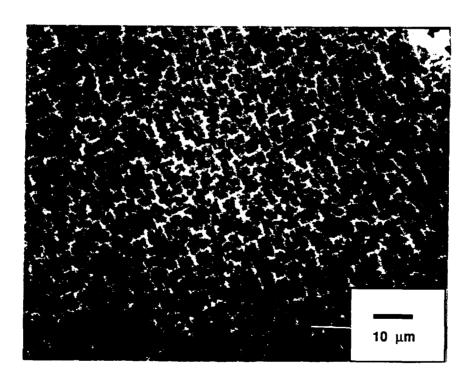
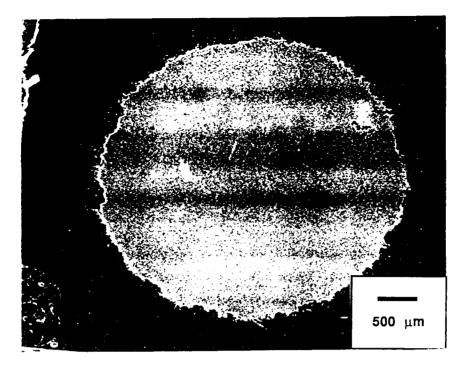


FIGURE 3. Run 52. SEM micrographs of film grown from 0.33% MTS/H2 at 1300°C.



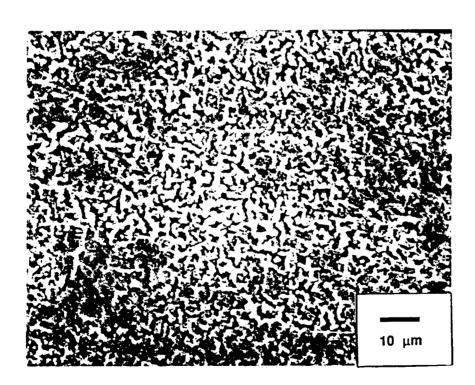
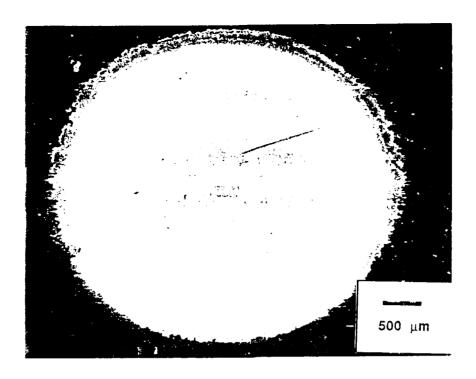


FIGURE 4. Run 53. SEM micrographs of film grown from 0.40% MTS/H2 at 1300°C.



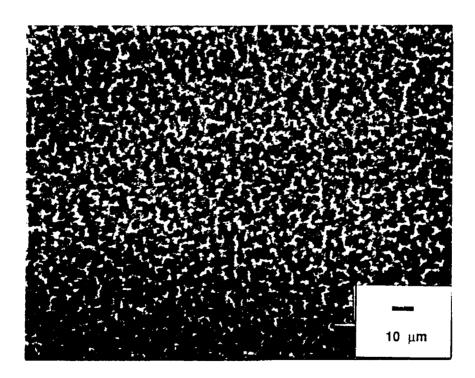
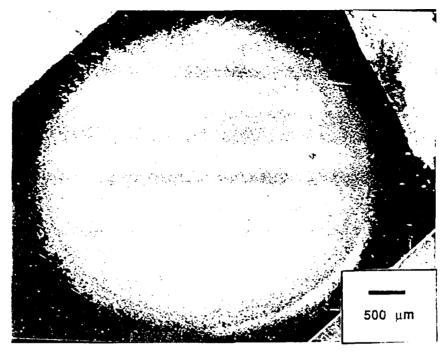


FIGURE 5. Run 59. SEM micrographs of film grown from 1.0% MTS/H2 at 1300°C.



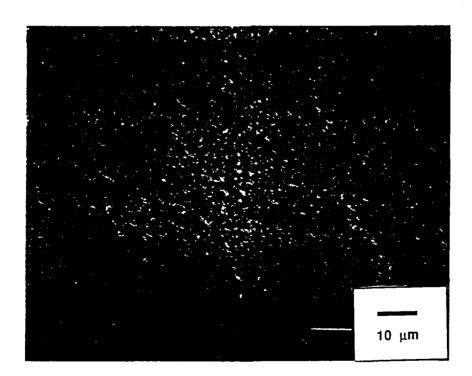
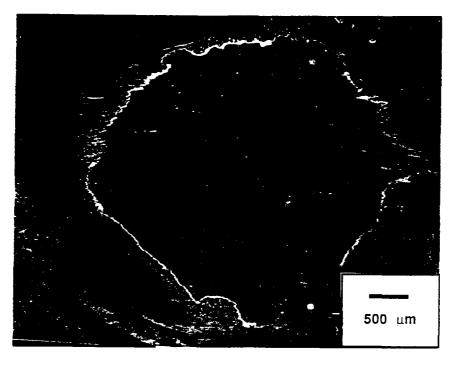


FIGURE 6. Run 60. SEM micrographs of film grown from 1.9% MTS/H2 at 1300°C.



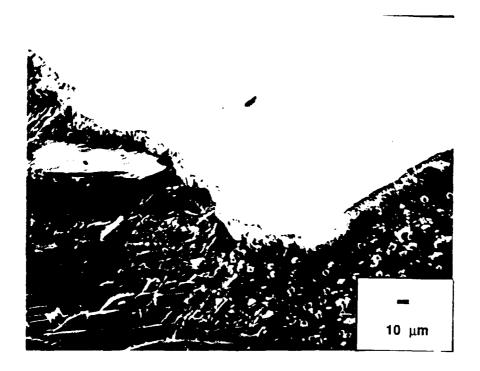
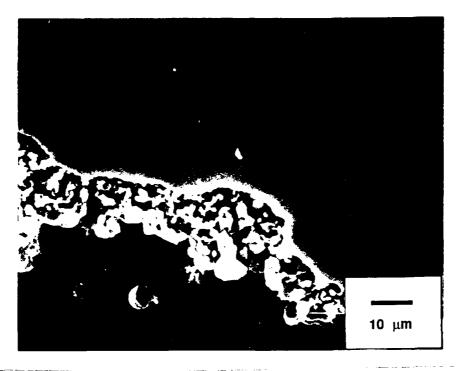


FIGURE 7. Run 63. Lower magnification SEM micrographs of film grown from 1.9% MTS/H2 at 1300 - 1400 $^{\circ}$ C.





B

FIGURE 8. Run 63. Higher magnification SEM micrographs of film grown from 1.9% MTS/H2 at 1300 - 1400°C.

view, as in Figure 3B, these early crystals are oriented cubically, with 90° angles clearly seen in Figure 3B.

The best result so far was run 63. Unfortunately, the belljar viewport used by the optical pyrometer to measure Si surface temperture during a run was occluded during run 63. Since optical pyrometer measurements automatically determines the power output from the rf power supply, rf output was boosted to compensate for a perceived loss of substrate temperature. The boosted rf power increased the substrate temperature to near the melting point of silicon (1410°C); after removal from the reactor, the perimeter of the silicon substrate was found to be partially melted.

There is evidence that run 63 may have been DMI's first heteroepitaxial β -SiC film on silicon. The film was optically transparent, with a very smooth and flat texture. The film had a slight greenish color under the optical microscope. Figures 7 and 8 indicate that the film was run long enough for the numerous subgrains to coalesce into a continuous single crystal. The numerous subgrains had a thickness of 4-6 μ m; the continuous smooth film atop the subgrains had a thickness under 1 μ m. Under careful inspection of Figures 7B and 8B, orange peel surface texture is discernable. This microstructure reflects the transition of the SiC film from the etched surface at the bottom of the silicon crater to the smoother, orange peel surface at the top of the film.

The Raman spectrum of film 63 was weak in intensity. The spectrum of Figure 9 indicates the presence of both α -SiC and β -SiC. A TO mode of α -SiC is observed at 786 cm⁻¹ and a TO mode of β -SiC is at 798 cm⁻¹. Despite total thicknes of the film being 5 - 7 μ m, the weak Raman response is puzzling. The film may contain a high concentrations of crystallograpic defects which reduce Raman intensity. The multiple subgrains seen in Figure 8B support this defective crystal theory. In future growth runs, DMI will attempt to grow films at a slower rate in order to improve the morphology and increase the crystallinity of the β -SiC monocrystals.

3.0 FUTURE WORK

DMI will work to finish the statement of work as summarized in Section 1 of this Report. The immediate goal will be to grow one or more monocrystalline β -SiC films to a thickness at least 30 μ m. The silicon wafer will then be selectively etched to create a freestanding β -SiC crystal.

DMI has installed a tube furnace with a fused silica liner. The furnace was installed with the necessary safety equipment to perform chlorinated thermal oxidation of silicon or silicon carbide. The exhaust from the furnace is plumbed with

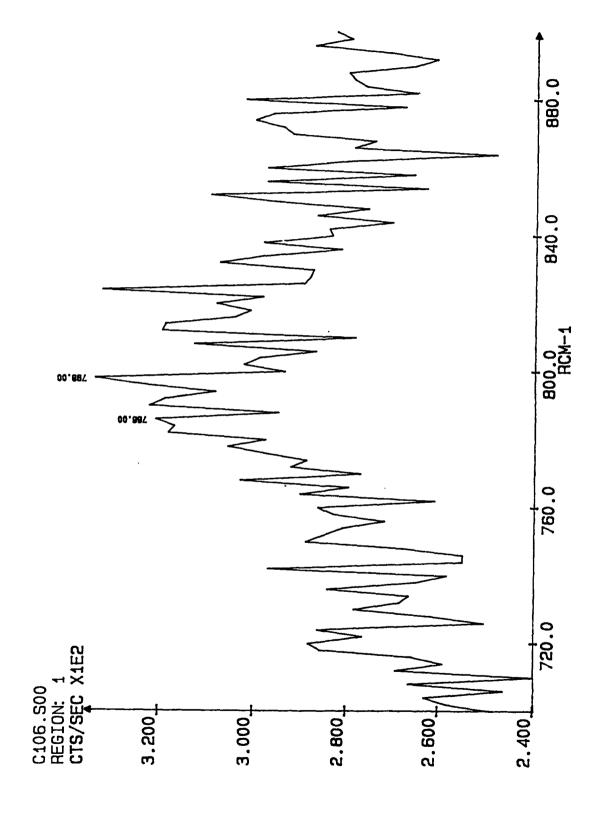


FIGURE 9. Raman spectrum of film grown by run 63. The TO mode of alpha silicon carbide is present at 786 cm-1 and the TO mode of beta silicon carbide is present at 798 cm-1.

Teflon tubing; a corrosion-resistant exhaust blower draws the effluent from the tube furnace into DMI's scrubber.

DMI will not use a traditional mixture of HCl gas plus O₂ to perform the chlorinated oxidation of \$\beta\$-SiC crystals. Instead, DMI will employ mixtures of trichloroethane (TCA) and O₂ using equipment supplied by J. C. Schumacher Co (JCS). DMI has a JCS M-dot bubbler filled with semiconductor-grade TCA. DMI will flow TCA/O₂ mixtures prescribed by JCS which can produce the same results as flowing between 1 to 10% HCl/H₂. TCA offers many safety advantages over HCl gas. TCA is a liquid which does not decompose into HCl until well inside the hot tube furnance; the TCA reacts with the O₂ to volatilize carbon as CO₂. Corrosion of the inlet tubing is minimized since TCA liquid or vapor is not very corrosive.